Mixed Suspension Mixed Product Removal Crystallization (MSMPR)



Ashfaq M Ansery Lecturer, ChE Deptt BUET







MSMPR Crystallizer

- □ An idealized crystallizer model
- Served well as a basis for identifying the kinetic parameters and showing how knowledge of them can be applied to calculate the performance of such a crystallizer

Assumptions

Steady state operation

- At all times the crystallizer contains a mixed-suspension magma, with no product classification
- At all times uniform super saturation exists throughout the magma

ΔL law applicable

Assumptions cont...

- No size-classified withdrawal system is used
- No crystals in the feed
- The product magma leaves the crystallizer in equilibrium, so the mother liquor in the product magma is saturated
- No crystal breakage into finite particle size occurs

Interpretation

- Constant nucleation rate at all points in the magma
- Constant growth rate and independent of crystal size and location
- All volume elements of mother liquor contain a mixture of particles ranging in size from nuclei to large particles

Particle size distribution is independent of location in the crystallizer and is identical to the size distribution in the product

Population-Density

- Basic quantity in the theory of the Crystal Size Distribution
- The population density n is defined as the slope of the cumulative distribution curve (N/V vs. L) at size L

Population-Density cont..

- $N \longrightarrow$ no of crystals of size L and smaller in the magma
- $V \longrightarrow$ volume of mother liquor in the magma
- $L \longrightarrow crystal size$

at L=0, N=0 $L=L_T, N=N_T$

Cumulative Distribution Curve



Population-Density cont..



at L=0, n=n⁰ at L=L_T, n=0

n E function of L and invariant in both time and location in the magma

Dimensions of *n*: Number/Volume-Length

Fundamental Relation of the MSMPR Crystallizer

n=n°e^{-z}



Population Density vs. Length



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Moment Equations

□ The normalized *j*th moment is defined by

 $\mu_{j} \equiv \frac{\int_{0}^{z} nz^{j} dz}{\int_{0}^{\infty} nz^{j} dz}$

Moment Equations cont..

□ Integrating for values of j=1 through j=3 gives $\mu_0=1-e^{-z}$ → number $\mu_1=1-(1-z)e^{-z}$ → Size $\mu_2=1-(1+z+\frac{1}{2}z^2)e^{-z}$ → Area $\mu_3=1-(1+z+\frac{1}{2}z^2+\frac{1}{6}z^3)e^{-z}$ → Mass

Moment Equations cont..

The differential distributions are

 $\frac{d\mu_0}{d\mu_0} = e^{-z}$ dz $\frac{d\mu_1}{z} = ze^{-z}$ dz $\frac{d\mu_{2}}{z} = \frac{z^{2}e^{-z}}{z}$ dz 2 $d\mu_{3}$ _ $z^{3}e^{-z}$ dz 6

Particle Technology

Size Distribution Relations



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Particle Technology

Predominant Crystal Size

 $\mu_3 = 1 - (1 + z + \frac{1}{2} z^2 + \frac{1}{6} z^3) e^{-z} \rightarrow \text{mass distribution } x_m$

 $\frac{d\mu_{3}}{d\mu_{3}} = \frac{z^{3}e^{-z}}{d\mu_{3}}$ dz = 6

at maximum

 $\frac{dx_m}{dx_m} = 0$ dz

 $-7^{3}e^{-z} + 37^{2}e^{-z} = 0$ 7 = 3*i.e. z*_{pr}=3